

1. Incompressible N-S & continuity Eqns, laminar flow  
 - 2D so,  $w=0$ , No press grad in horiz  
 fully developed (f.d.)

$$\frac{du}{dx} + \frac{dv}{dy} + \frac{dw}{dz} = 0$$

fully developed (f.d.)

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$

$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right)$$

$$u(x,0) = v(x,0) = 0$$

$$u(x,h) = U, v(x,h) = 0$$

$$\frac{du}{dx} + \frac{dv}{dy} = 0 \Rightarrow 0 \text{ since } v(x,0) = 0 \Rightarrow v(x,y) = 0 \quad (*)$$

$$0 = \nu \frac{d^2 u}{dy^2} \Rightarrow \text{Integrate Twice}$$

$$u(y) = Ay + B$$

$$u(0) = 0 \Rightarrow B = 0$$

$$u(h) = U \rightarrow A = \frac{U}{h}$$

$$u(y) = \frac{U}{h} y$$

(b) (1) Strain Rate tensor  $\Rightarrow S_{ij} = \frac{1}{2} \left( \frac{du_i}{dx_j} + \frac{du_j}{dx_i} \right)$

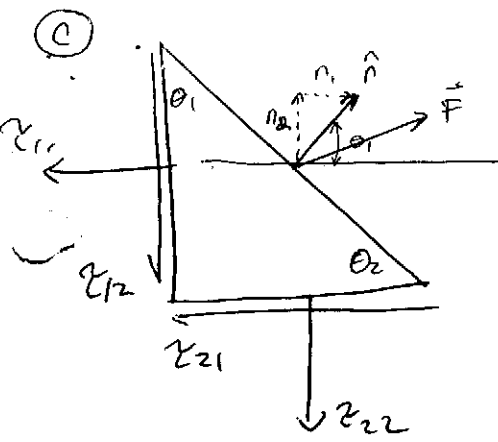
$$S_{ij} = \begin{pmatrix} S_{11} & S_{12} & S_{13} \\ S_{21} & S_{22} & S_{23} \\ S_{31} & S_{32} & S_{33} \end{pmatrix} = \begin{pmatrix} 0 & \frac{U}{2h} & 0 \\ \frac{U}{2h} & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \Rightarrow \text{Since only } \frac{du}{dy} \neq 0$$

$$S_{12} = \frac{1}{2} \frac{du_1}{dx_2} = \frac{1}{2} \frac{du}{dy} = \frac{U}{2h}$$

(2) Stress tensor  $\Rightarrow \sigma_{ij} = -p \delta_{ij} + \nu \left( \frac{du_i}{dx_j} + \frac{du_j}{dx_i} \right)$  (Incompressible flow so  $\frac{du_i}{dx_j} = 0$ )

$$\sigma_{ij} = \begin{pmatrix} -p & \frac{\nu U}{h} & 0 \\ \frac{\nu U}{h} & -p & 0 \\ 0 & 0 & -p \end{pmatrix}$$

(2)



$$\vec{F} = f_i$$

$$\tau_{ij} = \begin{bmatrix} 0 & \mu \frac{\sigma}{h} \\ \mu \frac{\sigma}{h} & 0 \end{bmatrix}$$

Force per unit Area:

$$f_i = n_j \tau_{ji}$$

$$f_1 = n_1 \tau_{11} + n_2 \tau_{21} \quad \text{but } \tau_{11} = \tau_{22} = 0$$

$$f_2 = n_1 \tau_{12} + n_2 \tau_{22}$$

$$n_1 = \cos \theta_1 = \cos(50^\circ) = 0.6428$$

$$n_2 = \cos \theta_2 = \cos(40^\circ) = 0.766$$

$$f_1 = n_2 \tau_{21} = 0.766 \mu \frac{\sigma}{h}$$

$$f_2 = n_1 \tau_{12} = 0.6428 \mu \frac{\sigma}{h}$$

$$\Rightarrow |f| = (f_1^2 + f_2^2)^{1/2} = \mu \frac{\sigma}{h}$$

$$\left. \begin{aligned} \sin \phi &= \frac{f_2}{|f|} = 0.6428 \\ \cos \phi &= \frac{f_1}{|f|} = 0.766 \end{aligned} \right\} \phi = 40^\circ$$

(d) Viscous Dissipation,  $\Phi$  for an incompressible flow

$$\phi = 2\mu S_{ij} S_{ij} = \frac{\mu}{2} \left( \frac{du_i}{dx_j} + \frac{du_j}{dx_i} \right)^2$$

$$= 2\mu \left( S_{11}^2 + S_{21}^2 + S_{12}^2 + S_{22}^2 + S_{23}^2 + S_{32}^2 + S_{33}^2 \right)$$

$$= 2\mu (S_{21}^2 + S_{12}^2) = 2\mu \left( \frac{U^2}{4h^2} + \frac{U^2}{4h^2} \right)$$

$$\boxed{\phi = \mu \frac{U^2}{h^2}}$$

$$\textcircled{e} \int_{cv} \frac{dE}{dt} dV + \int_{cs} E(\vec{v} \cdot \vec{n}) dA = \int_{cs} \rho(\vec{g} \cdot \vec{v}) dV + \int_{cs} u_j \sigma_{ij} n_i dA + \int_V p(\vec{\nabla} \cdot \vec{v}) dV - \int_{cv} \phi dV \quad \textcircled{3}$$

Where  $E = \rho \frac{U_i^2}{2} \rightarrow$  Kinetic Energy per unit volume

$\textcircled{A} = 0 \Rightarrow$  steady flow

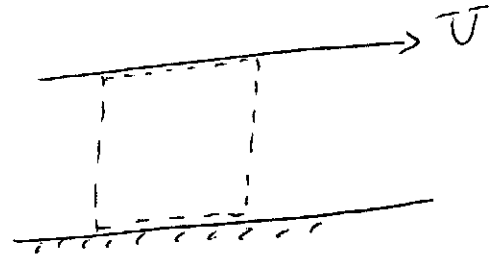
$\textcircled{B} = 0 \Rightarrow$  fully developed

$\textcircled{C} = 0 \Rightarrow$  Neglect hydrostatic

$\textcircled{D} \Rightarrow$  Include

$\textcircled{E} \Rightarrow 0 \Rightarrow$  Incompressible flow

$\textcircled{F} \Rightarrow$  Include

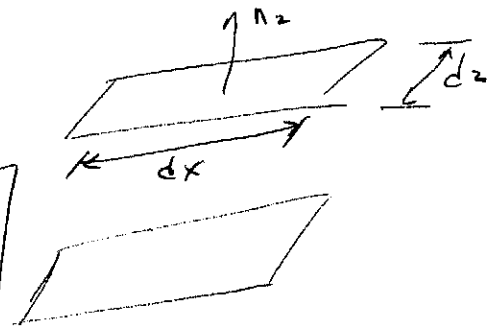


$$\int_{cs} u_j \sigma_{ij} n_i dA = \int_{cv} \phi dV$$

Pressure terms cancel out so we are left with

$$\int_{cs} u_1 \sigma_{z1} n_z dx dz = \int_{cv} \rho \frac{U^2}{h} dx dy dz$$

$$\iint U \left( \rho \frac{U}{h} \right) dx dy = \iiint \rho \frac{U^2}{h} dx dz$$



$\rightarrow$

f.  $\frac{dP}{dx} = a$ , Couette flow with axial pressure gradient

(4)

$$\mu \frac{d^2 u}{dy^2} = \frac{dP}{dx} = a$$

3

$$\frac{d^2 u}{dy^2} = \frac{a}{\mu}$$

$$\frac{du}{dy} = \frac{a}{\mu} y + B$$

$$u = \frac{a}{\mu} \frac{y^2}{2} + By + C$$

boundary conditions

$$u(y=0) = 0 \quad (1)$$

$$u(y=h) = U \quad (2)$$

B.C. 1  $\rightarrow C = 0$

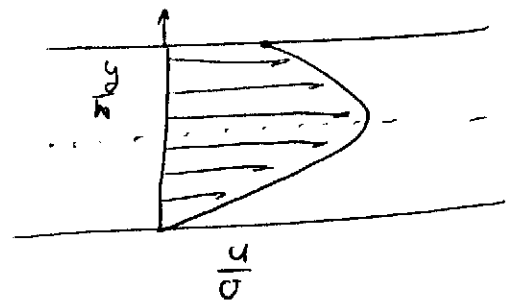
B.C. 2

$$U = \frac{a}{\mu} \frac{h^2}{2} + Bh$$

$$B = \frac{U}{h} - \frac{a}{\mu} \frac{h}{2}$$

$$u = \frac{a}{\mu} \frac{y^2}{2} + \left( \frac{U}{h} - \frac{a}{\mu} \frac{h}{2} \right) y$$

$$u(y) = \frac{a}{2\mu} (y^2 - yh) + \frac{Uy}{h}$$



9) Just like problem c except now  $\tau_{ij} = \mu \left( \frac{du_i}{dx_j} + \frac{du_j}{dx_i} \right)$  is

$$\tau_{ij} = \begin{bmatrix} 0 & \mu \frac{du}{dy} & 0 \\ \mu \frac{du}{dy} & 0 & 0 \\ 0 & 0 & 0 \end{bmatrix}$$

$$\frac{du}{dy} = \frac{a}{\mu} (2y - h) + \frac{U}{h}$$

Since  $n_1 = \frac{1}{2}$  and  $n_2 = 0.866$  are unchanged ~~\_\_\_\_\_~~

$$f_1 = 0.866 \left( \frac{a}{\mu} (2y - h) + \frac{U}{h} \right)$$

$$f_2 = \frac{1}{2} \left( \frac{a}{\mu} (2y - h) + \frac{U}{h} \right)$$

$$f = (f_1^2 + f_2^2)^{1/2}$$

$$\sin \phi = \frac{f_2}{f}$$

$$\cos \phi = \frac{f_1}{f}$$

Three-Dimensional Incompressible Flow

Four variables or unknowns:

- Pressure  $P$
- Three components of velocity  $\vec{V}$

Four equations of motion:

- Continuity,  $\vec{\nabla} \cdot \vec{V} = 0$
- Three components of Navier–Stokes,  $\rho \frac{D\vec{V}}{Dt} = -\vec{\nabla}P + \rho\vec{g} + \mu\nabla^2\vec{V}$

FIGURE 9-43

A general three-dimensional but incompressible flow field with constant properties requires four equations to solve for four unknowns.

## 9-6 • DIFFERENTIAL ANALYSIS OF FLUID FLOW PROBLEMS

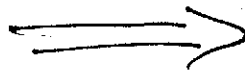
In this section we show how to apply the differential equations of motion in both Cartesian and cylindrical coordinates. There are two types of problems for which the differential equations (continuity and Navier–Stokes) are useful:

- Calculating the pressure field for a known velocity field
- Calculating both the velocity and pressure fields for a flow of known geometry and known boundary conditions

For simplicity, we consider only incompressible flow, eliminating calculation of  $\rho$  as a variable. In addition, the form of the Navier–Stokes equation derived in Section 9-5 is valid only for Newtonian fluids with constant properties (viscosity, thermal conductivity, etc.). Finally, we assume negligible temperature variations, so that  $T$  is not a variable. We are left with four variables or unknowns (pressure plus three components of velocity), and we have four differential equations (Fig. 9-43).

### Calculation of the Pressure Field for a Known Velocity Field

The first set of examples involves calculation of the pressure field for a known velocity field. Since pressure does not appear in the continuity equation, we can theoretically generate a velocity field based solely on conservation of mass. However, since velocity appears in both the continuity equation and the Navier–Stokes equation, these two equations are *coupled*. In addition, pressure appears in all three components of the Navier–Stokes equation, and thus the velocity and pressure fields are also coupled. This intimate coupling between velocity and pressure enables us to calculate the pressure field for a known velocity field.



#### EXAMPLE 9-13 Calculating the Pressure Field in Cartesian Coordinates

Consider the steady, two-dimensional, incompressible velocity field of Example 9-9, namely,  $\vec{V} = (u, v) = (ax + b)\mathbf{i} + (-ay + cx)\mathbf{j}$ . Calculate the pressure field as a function of  $x$  and  $y$ .

**SOLUTION** For a given velocity field, we are to calculate the pressure field. **Assumptions** 1 The flow is steady. 2 The fluid is incompressible with constant properties. 3 The flow is two-dimensional in the  $xy$ -plane. 4 Gravity does not act in either the  $x$ - or  $y$ -direction.

**Analysis** First we check whether the given velocity field satisfies the two-dimensional, incompressible continuity equation:

$$\underbrace{\frac{\partial u}{\partial x}}_a + \underbrace{\frac{\partial v}{\partial y}}_{-a} + \underbrace{\frac{\partial w}{\partial z}}_{0 \text{ (2-D)}} = a - a = 0$$

Problem # 2

Thus, continuity was not satisfied. Next, we can

$$\rho \left( \frac{\partial v}{\partial t} + v \frac{\partial v}{\partial y} \right)$$

(steady)

The y-momentum

The y-momentum equation reduces to

The x-momentum equation

In order to calculate the pressure field, we require that the matter (Fig. 9-2 and 3, respectively)

$$\frac{\partial^2 P}{\partial x^2}$$

Equation 4 is the Navier–Stokes equation

If at this point we yield two in Eq. 9-44 were not satisfied, we could not solve the equation, at least for the velocity field.

To calculate the pressure field, we obtain an expression for the pressure field.

Note that we have a constant of integration in the partial derivative.

continuity is indeed satisfied by the given velocity field. If continuity is satisfied, we would stop our analysis—the given velocity field would be physically possible, and we could not calculate a pressure field. We consider the y-component of the Navier–Stokes equation:

$$\rho \left( \frac{\partial v}{\partial t} + v \frac{\partial v}{\partial x} + w \frac{\partial v}{\partial z} \right) = -\frac{\partial p}{\partial y} + \mu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial z^2} \right) + \rho g_y$$

where  $\rho$  is the density,  $\mu$  is the dynamic viscosity, and  $\rho g_y$  is the y-component of the body force. In this case,  $v = 0$ ,  $w = 0$ , and  $\rho g_y = 0$ . The equation reduces to

$$0 = -\frac{\partial p}{\partial y} + \mu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial z^2} \right)$$

$$\frac{\partial p}{\partial y} = \rho(-ax - bc - a^2y + ax) = \rho(-bc - a^2y) \quad (2)$$

momentum equation is satisfied, provided we can generate a pressure field that satisfies Eq. 2. In similar fashion, the x-momentum equation

$$\frac{\partial p}{\partial x} = \rho(-a^2x - ab) \quad (3)$$

momentum equation is also satisfied, provided we can generate a pressure field that satisfies Eq. 3.

For a physically realistic steady, incompressible flow field requires a smooth field  $P(x, y)$  that is a smooth function of  $x$  and  $y$  (there can be no discontinuities in either  $P$  or a derivative of  $P$ ). Mathematically, this means that the order of differentiation ( $x$  then  $y$  versus  $y$  then  $x$ ) should not matter. We check whether this is so by cross-differentiating Eqs. 2 and 3, respectively,

$$\frac{\partial}{\partial x} \left( \frac{\partial p}{\partial y} \right) = 0 \quad \text{and} \quad \frac{\partial}{\partial y} \left( \frac{\partial p}{\partial x} \right) = 0 \quad (4)$$

Eq. 4 shows that  $P$  is a smooth function of  $x$  and  $y$ . Thus, the given velocity field satisfies the steady, two-dimensional, incompressible Navier–Stokes equation.

In the point in the analysis, the cross-differentiation of pressure were to be incompatible relationships. In other words, if the equation in Fig. 9-44 were not satisfied, we would conclude that the given velocity field does not satisfy the steady, two-dimensional, incompressible Navier–Stokes equation, and we would abandon our attempt to calculate a steady pressure field and try to calculate a different velocity field.

To calculate  $P(x, y)$ , we partially integrate Eq. 2 (with respect to  $y$ ) to obtain an expression for  $P(x, y)$ .

$$P(x, y) = p \left( -bcy - \frac{a^2y^2}{2} \right) + g(x) \quad (5)$$

where we add an arbitrary function of the other variable  $x$  rather than a constant of integration, since this is a partial integration. We then take the derivative of Eq. 5 with respect to  $x$  to obtain

$$\frac{\partial p}{\partial x} = g'(x) = \rho(-a^2x - ab) \quad (6)$$

**FIGURE 9-44** For a two-dimensional flow field in the  $xy$ -plane, cross-differentiation reveals whether pressure  $P$  is a smooth function.

Cross-Differentiation,  $xy$ -Plane  
 $\frac{\partial^2 p}{\partial x \partial y} = \frac{\partial^2 p}{\partial y \partial x}$   
 does not matter.  
 only if the order of differentiation  
 $P(x, y)$  is a smooth function of  $x$  and  $y$

s of motion in  
 es) are useful.

ating calcula-  
 takes equation  
 with constant  
 assume negli-  
 left with four  
 (city), and we

are field for a  
 continuity equa-  
 y on conserva-  
 continuity equa-  
 re coupled. In  
 Navier–Stokes  
 coupled. This  
 o calculate the

id of Example  
 the pressure

pressure field.  
 ble with con-  
 ne. 4 Gravity  
 sifies the two-

(1)

where we have equated our result to Eq. 3 for consistency. We now integrate Eq. 6 to obtain the function  $g(x)$ :

$$g(x) = \rho \left( -\frac{a^2 x^2}{2} - abx \right) + C_1 \quad (7)$$

where  $C_1$  is an arbitrary constant of integration. Finally, we substitute Eq. 7 into Eq. 5 to obtain our final expression for  $P(x, y)$ . The result is

$$P(x, y) = \rho \left( -\frac{a^2 x^2}{2} - \frac{a^2 y^2}{2} - abx - bcy \right) + C_1 \quad (8)$$

**Discussion** For practice, and as a check of our algebra, you should differentiate Eq. 8 with respect to both  $y$  and  $x$ , and compare to Eqs. 2 and 3. In addition, try to obtain Eq. 8 by starting with Eq. 3 rather than Eq. 2; you should get the same answer.

Notice that the final equation (Eq. 8) for pressure in Example 9-13 contains an arbitrary constant  $C_1$ . This illustrates an important point about the pressure field in an incompressible flow; namely,

The velocity field in an incompressible flow is not affected by the absolute magnitude of pressure, but only by pressure differences.

This should not be surprising if we look at the Navier–Stokes equation, where  $P$  appears only as a *gradient*, never by itself. Another way to explain this statement is that it is not the absolute magnitude of pressure that matters, but only pressure *differences* (Fig. 9-45). A direct result of the statement is that we can calculate the pressure field to within an arbitrary constant, but in order to determine that constant ( $C_1$  in Example 9-13), we must measure (or otherwise obtain)  $P$  somewhere in the flow field. In other words, we require a pressure boundary condition.

We illustrate this point with an example generated using **computational fluid dynamics (CFD)**, where the continuity and Navier–Stokes equations are solved numerically (Chap. 15). Consider downward flow of air through a channel in which there is a nonsymmetrical blockage (Fig. 9-46). (Note that the computational flow domain extends much further upstream and downstream than shown in Fig. 9-46.) We calculate two cases that are identical except for the pressure condition. In case 1 we set the gage pressure downstream of the blockage to zero. In case 2 we set the pressure at the same location to 500 Pa gage pressure. The gage pressure at the top center of the field of view and at the bottom center of the field of view are shown in Fig. 9-46 for both cases, as generated by the two CFD solutions. You can see that the pressure field for case 2 is identical to that of case 1 except that the pressure is everywhere increased by 500 Pa. Also shown in Fig. 9-46 are a velocity vector plot and a streamline plot for each case. The results are identical, confirming our statement that the velocity field is not affected by the absolute magnitude of the pressure, but only by pressure *differences*. Subtracting the pressure at the bottom from that at the top, we see that  $\Delta P = 12.784$  Pa for both cases.

The statement about pressure differences is *not* true for *compressible* flow fields, where  $P$  is the thermodynamic pressure rather than the mechanical pressure. In such cases,  $P$  is coupled with density and temperature through

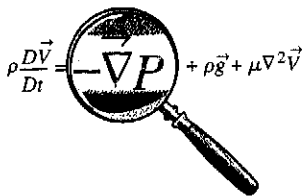


FIGURE 9-45

Since pressure appears only as a gradient in the incompressible Navier–Stokes equation, the absolute magnitude of pressure is not relevant—only pressure *differences* matter.

an equation of compressible :  
vation equatio  
of state.

We take this in Fig. 9-46. :  
relatively sim  
occurs across  
downstream o  
corner, and th  
streamlines in  
downstream o  
The velocity v  
the opening—  
of the geomet  
wall much soe  
the region wh  
Finally, notice  
streamlines co  
downstream, t  
lines in the re  
ties are relativ

Finally, we  
gration of the  
Instead, some  
commonly u  
Navier–Stokes  
ity equation.  
form of **Poiss**  
tion ( $n$ ) to the

Poisson's equat

Then, as the  
equation is us  
values at itera

Correction for i

Details associ  
beyond the sc  
is developed i

**EXAMPLE 9-**

Consider the  
ple 9-5 with  
axis lies alo  
 $u_r = 0$  and  
function of  $t$

**SOLUTION**

```
%Homework 2, problem 2
clear;
clc;
rho = 1 %kg/m^3
C1 = 0 %Pa
[x,y] = meshgrid(-1:.1:1,-1:.1:1);
a = 1;
b = 1;
c =1;
%calculate u-velocity
u=a*x + b;
%calculate v-velocity
v = -a*y+ c*x;

%Now plot pressure contours
P = rho*(-(a^2*x.^2)/2 - (a^2*y.^2)/2 -a*b*x - b*c*y) + C1;
hold
contourf(x,y,P)
%create velocity vector plot
quiver(x,y,u,v, '-k')
colorbar
```



Pressure Contours and Velocity Vectors

